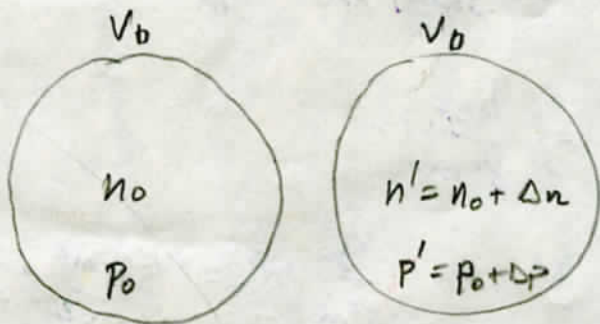


# ISOTHERMAL IDEAL GAS

$$PV = nRT$$

A.



How much does pressure change if number of moles is increased (at constant volume)

$$P_0 V_0 = n_0 RT$$

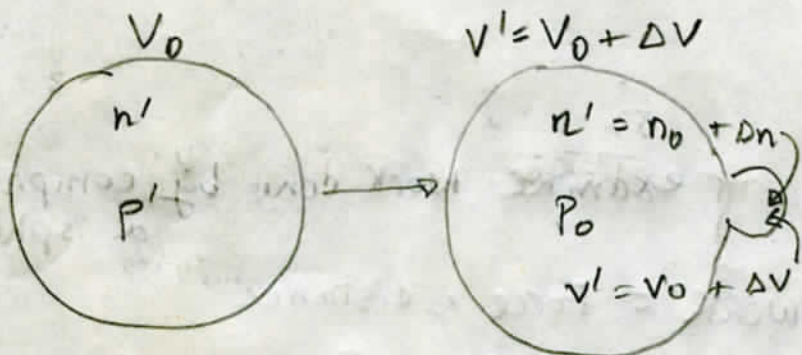
$$P' V_0 = n' RT$$

$$\text{so } \frac{P'}{P_0} = \frac{n'}{n_0}$$

$$\Delta n = n' - n_0 = \left( \frac{P'}{P_0} - 1 \right) n_0$$

now, since we know  $P_0 = 100 \text{ MPa}$  and  $\Delta P = 5 \text{ MPa}$ , we can infer  $\Delta n$

B.



How much does volume change if volume is expanded enough to reduce pressure  $\Delta P$ ? (at const number of moles)

$$P' V_0 = n' RT$$

$$V' = \frac{n' RT}{P_0} =$$

$$n_0 \frac{P' RT}{P_0 P_0} = \frac{n_0 RT P'}{P_0^2} = V'$$

C. How much energy is released when  $n'$  moles of gas expanded from  $V_0$  to  $V'$ ?

$$E = \int_{V_0}^{V'} P(V) dV = n' RT \int_{V_0}^{V'} \frac{dV}{V} = n' RT (\ln V' - \ln V_0) = n' RT \ln \frac{V'}{V_0} =$$

$$\frac{V'}{V_0} = \frac{n_0 RT P'}{P_0^2} \frac{P_0}{n_0 RT} = \frac{P'}{P_0}$$

$$E = n' RT \ln \frac{P'}{P_0}$$

D. How many moles,  $n'$ , of gas are in a volume  $V_0$  at pressure  $P'$ ?

$$P' V_0 = n' RT \quad n' = \frac{P' V_0}{RT}$$

$$\text{so } E = P' V_0 \ln \frac{P'}{P_0}$$

E. Energy Calculation (2.5% porosity)

$$V_0 = \frac{4}{3} \pi (1500)^3 \cdot 0.025 \text{ m}^3 = 3.53 \times 10^8 \text{ m}^3$$

$$P' = 134 \times 10^6 \text{ Pa} \quad \frac{\text{kg m}}{\text{s}^2 \text{ m}^2} = \frac{\text{kg}}{\text{s}^2 \text{ m}}$$

$$P_0 = 130 \times 10^6 \text{ Pa}$$

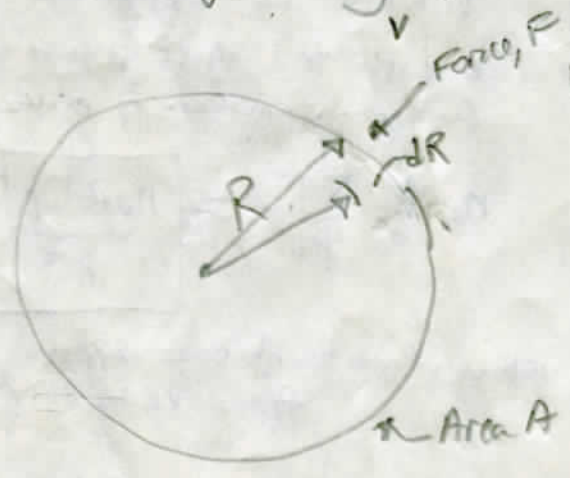
$$\frac{P'}{P_0} = \frac{134}{130}$$

$$PV \rightarrow \frac{\text{kg}}{\text{s}^2 \text{ m}} \text{ m}^3 = \text{kg} \frac{\text{m}^2}{\text{s}^2} = J$$

$$\text{note } j = \frac{\text{kg m}^2}{\text{s}^2}$$

$$E = P' V_0 \ln\left(\frac{P'}{P_0}\right) = (134 \times 10^6) (3.53 \times 10^8) (3.03 \times 10^{-2}) = 1.43 \times 10^{15} \text{ J}$$

F. Proof of  $E = \int_V P dV$  examine work done by compressing a sphere.



WORK = Force  $\cdot$  distance

$$dE = F \cdot dR$$

since  $F = PA$

$$= PA \cdot dR$$

$$= P A dR = P dV$$

since  $dV = A dR$

G. Note  $\ln(1+\epsilon) \approx \epsilon$  so  $\ln\left(\frac{P'}{P_0}\right) = \ln\left(\frac{P_0 + \Delta P}{P_0}\right) = \ln\left(1 + \frac{\Delta P}{P_0}\right)$

$$\text{so } E = P' V_0 \ln\left(\frac{P'}{P_0}\right) \approx \frac{P'}{P_0} \Delta P V_0 \approx \Delta P V_0 \approx \frac{\Delta P}{P_0}$$

$$(4 \times 10^6) (3.5 \times 10^8) = 1.4 \times 10^{15} \text{ J}$$

# G. Energy Delivered by Seismic Waves

Plane SA wave  $\underline{u} = A \begin{pmatrix} 0 \\ 1 \\ 0 \end{pmatrix} e^{i\omega(\frac{x}{\beta} - t)}$  of strain  
=  $\epsilon = 10^{-5}$

velocity  $\dot{u}_y = -i\omega A e^{i\omega(\frac{x}{\beta} - t)}$

strain  $\epsilon_{21} = \frac{1}{2} u_{y,x} = \frac{i\omega A}{2\beta} e^{i\omega(\frac{x}{\beta} - t)} = \epsilon e^{i\omega(\frac{x}{\beta} - t)}$

$\epsilon = \frac{i\omega A}{2\beta}$  so  $i\omega A = 2\beta \epsilon$

(note not dependent on pressure)

$\dot{u}_y = -2\beta \epsilon e^{i\omega(\frac{x}{\beta} - t)}$

mean energy flux  $= \rho \beta \langle \dot{u}_y^2 \rangle = \frac{1}{2} \rho \beta \dot{u}_{y,max}^2 = \frac{1}{2} \rho \beta 4\beta^2 \epsilon^2 = 2\rho \beta^3 \epsilon^2$

energy thru disk of Radius  $R$  in time  $T$

$E = 2\rho \beta^3 \epsilon^2 \pi R^2 T = 2\pi \rho \beta^3 \epsilon^2 R^2 T$

$= 2\pi (2500) (3000)^3 (10^{-5})^2 (1500)^2 30 = 2.86 \times 10^{12} \text{ J}$

$\frac{\text{kg}}{\text{m}^3} \frac{\text{m}^3}{\text{s}^3} \text{m}^2 \text{s} = \frac{\text{kg m}^2}{\text{s}^2} = \text{J}$

## H. Results

$\epsilon = 10^{-5}$

$m = 8$  eq at 150 km

$E_{\text{seismic wave}}$

$2.9 \times 10^{12} \text{ J}$

$1.5 \times 10^{14} \text{ J}$

$E_{\text{compressed gas}}$

$1.43 \times 10^{15} \text{ J}$

$\times E_{\text{compressed magma}}$

$9.7 \times 10^{14} \text{ J}$

## H. Energy in The magma fluid

$$\text{Energy density} = \frac{1}{2} T_{ij} \epsilon_{ij} = \frac{3}{2} c p = \frac{3}{2} \frac{p^2}{\lambda} = \frac{3}{2} \frac{\rho^2}{\rho \alpha^2}$$

$$\epsilon_{ij} = c \delta_{ij}$$

$$T_{ij} = p \delta_{ij}$$

$$p = \lambda c \quad c = p/\lambda$$

$$\rho \alpha^2 = \lambda$$

$$DE = \frac{3}{2} \frac{[(154 \cdot 10^6)^2 - (137000)^2]}{(2500)(3000)^2}$$

$$= \frac{3}{2} \frac{1056 \times 10^{12}}{2500 \cdot (3000)^2}$$

$$= 7.04 \times 10^4 \text{ j/m}^3$$

$$E = \text{Volume} \cdot \text{Energy density}$$

1-porosity

$$= \frac{4}{3} \pi (1500)^3 (0.975) 7.04 \times 10^4 = 9.70 \times 10^{14} \text{ j}$$

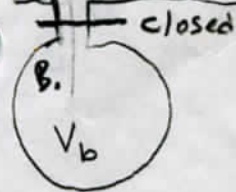
## I. Radiated energy according to Richter

$$\log E = 5.8 + 2.4 m \quad \text{in case}$$

Gives  $10^{18}$  j for  $m=8$  say  $E_R$  is 150 km from volcano

$$E_{mc} = \frac{10^{18} \cdot \pi (1500)^2}{\frac{2}{3} \pi (150000)^2} = \frac{3}{2} \left(\frac{1.5}{150}\right)^2 \cdot 10^{18} = \frac{3}{2} \times 10^{14} = 1.5 \times 10^{14} \text{ j}$$

A,  $V_a$ ,  $P_0$ ,  $n_a$



① How many moles,  $\Delta n$ , must one move from B. to A. to increase pressure in A. from  $P_0$  to  $P_0 + \Delta P$ ?

$$P_0 V_a = n_a RT$$

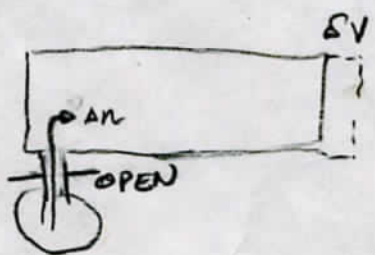
$$(P_0 + \Delta P) V_a = (n_a + \Delta n) RT$$

$$\Delta P V_a = \Delta n RT$$

$$\Delta P \frac{V_a}{n_a RT} = \frac{\Delta n}{n_a}$$

$$\frac{\Delta P}{P_0} = \frac{\Delta n}{n_a}$$

② How much one must expand a to move  $\Delta n$  moles from b to a? Say this causes a pressure drop,  $\Delta P$  and volume increase  $\Delta V$



Before

$$P_0 V_a = n_a RT$$

$$P_0 V_b = n_b RT$$

$$P_0 V_T = n_T RT ; V_T = V_a + V_b, n_T = n_a + n_b$$

after

$$(P_0 - \Delta P)(V_T + \Delta V) = n_T RT$$

$$P_0 - \Delta P = \frac{n_T RT}{V_T} \left(1 + \frac{\Delta V}{V_T}\right)^{-1} \approx P_0 \left(1 - \frac{\Delta V}{V_T}\right)$$

$$\frac{\Delta P}{P_0} = \frac{\Delta V}{V_T}$$

the change in moles in b is  $\frac{\Delta P}{P_0} = \frac{\Delta n}{n_b}$  (from #1)

$$\frac{\Delta P}{P_0} = \frac{\Delta n}{n_b} = \frac{n_a}{n_b} \frac{\Delta P}{P_0} = \frac{\Delta V}{V_T}$$

$$\Delta V = \frac{n_a}{n_b} \frac{\Delta P}{P_0} V_T$$

$V_T = V_a + V_b$  note  $\frac{n_a}{n_b} V_T = \frac{V_a}{V_b} (V_a + V_b)$

$$= \frac{V_a^2}{V_b} + V_a = V_a \left(1 + \frac{V_a}{V_b}\right)$$

$$\frac{\Delta V}{V_a} = \frac{\Delta P}{P_0} \left(1 + \frac{V_a}{V_b}\right)$$

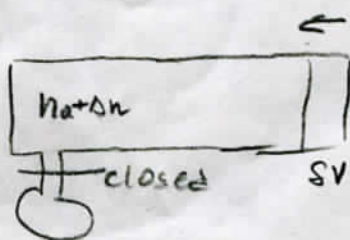
$\frac{n_a}{n_b} = \frac{V_a}{V_b}$

③ How much work is done by this expansion?

$$E_1 = \int_{V_T}^{V_T + \delta V} p dV = n_T RT \int_{V_T}^{V_T + \delta V} \frac{dV}{V} = n_T RT \ln\left(\frac{V_T + \delta V}{V_T}\right) = n_T RT \ln\left(1 + \frac{\delta V}{V_T}\right)$$

$$\approx n_T RT \frac{\delta V}{V_T} = P_0 \delta V = P_0 V_T \frac{n_a}{n_b} \frac{\Delta P}{P_0} = \frac{n_a}{n_b} V_T \Delta P = V_a \Delta P \left(1 + \frac{V_a}{V_b}\right)$$

④ Valve closed and A compressed back to volume  $V_a$ . This brings the pressure to  $P_0 + \Delta P$  in A. How much work?



in A

$$p = \frac{(n_a + \Delta n) RT}{V}$$

$$E_2 = - \int_{V_a}^{V_a + \delta V} p dV = - (n_a + \Delta n) RT \int_{V_a}^{V_a + \delta V} \frac{dV}{V} = - (n_a + \Delta n) RT \ln\left(\frac{V_a + \delta V}{V_a}\right) \approx - (n_a + \Delta n) RT \frac{\delta V}{V_a}$$

but  $\frac{(n_a + \Delta n) RT}{V_a} = P_0 + \Delta P$  so

$$E_2 = - (P_0 + \Delta P) \delta V = - (P_0 + \Delta P) V_T \frac{n_a}{n_b} \frac{\Delta P}{P_0}$$

⑤ TOTAL  $E$

$$E = E_1 + E_2 = P_0 V_T \frac{n_a}{n_b} \frac{\Delta P}{P_0} - (P_0 + \Delta P) V_T \frac{n_a}{n_b} \frac{\Delta P}{P_0} =$$

$$- \Delta P V_T \frac{n_a}{n_b} \frac{\Delta P}{P_0} = - \Delta P V_a \left(1 + \frac{V_a}{V_b}\right) \frac{\Delta P}{P_0}$$

## Case of infinite $V_b$

moles needed to increase pressure at constant volume

$$(P_0 + \Delta P) V_a = (n_a + \Delta n) RT \quad (\text{after})$$

$$P_0 V_a = n_a RT \quad (\text{before})$$

subtract  $\Delta P V_a = \Delta n RT$

$$\Delta P = \frac{\Delta n RT}{V_a} = \frac{\Delta n}{n_a} \frac{RT n_a}{V_a} = \frac{\Delta n}{n_a} P_0$$

$$\frac{\Delta P}{P_0} = \frac{\Delta n}{n_a}$$

note  $\Delta n RT = V_a \Delta P$

2. isobaric expansion by  $\delta V$  to bring in  $\Delta n$  moles



$$P_0 \delta V = \Delta n RT = \Delta P V_a$$

$$\frac{\Delta P}{P_0} = \frac{\delta V}{V_a}$$

$$\delta V = \frac{\Delta P}{P_0} V_a$$

3. work done on expansion:

$$E_1 = \int_{V_a}^{V_a + \delta V} P dV = P_0 \int_{V_a}^{V_a + \delta V} dV = P_0 \delta V$$

4. work done in compression, reservoir disconnected

$$E_2 = - \int_{V_a}^{V_a + \delta V} P(V) dV = -(n_a + \Delta n) RT \ln\left(1 + \frac{\delta V}{V_a}\right)$$

but  $(P_0 + \Delta P) V_a = (n_a + \Delta n) RT$

$$\approx -(P_0 + \Delta P) V_a \frac{\delta V}{V_a}$$

$$= -P_0 \delta V - \Delta P \delta V$$

$$5. (E_1 + E_2) = -\Delta P \delta V = -\Delta P \frac{\Delta P}{P_0} V_a$$

This checks with complete calc.

$$\lim_{V_b \rightarrow \infty} -\Delta P \frac{\Delta P}{P_0} V_a \left(1 + \frac{V_a}{V_b}\right) = -\Delta P V_a \left(\frac{\Delta P}{P_0}\right)$$

$$\ddot{u}_i = -\frac{1}{3} P_{3i} + \frac{1}{3} f_i$$

$$-\ddot{u}_{i,i} = +\frac{1}{3} P_{3ii} + \frac{1}{3} f_{i,i} \quad (\rho \text{ const})$$

$$u_{i,i} = -\frac{P}{\lambda}$$

$$\left(\frac{P}{\lambda}\right) = \ddot{q} = -\ddot{u}_{i,i} = \frac{1}{3} P_{3ii} + \frac{1}{3} f_{i,i}$$

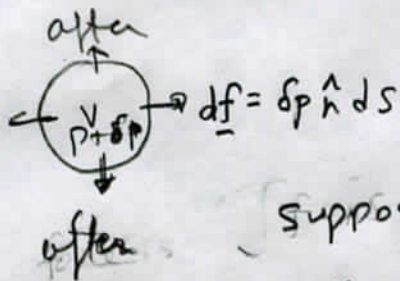
$$\ddot{q} = \frac{1}{3} \nabla^2 P + \frac{1}{3} \nabla \cdot f \quad q = \frac{P}{\lambda}$$

$$pV = nRT$$

inject gas

$$V_0 P$$

before



$$\delta p = \delta n \frac{RT}{V_b}$$

suppose  $\nabla \cdot f = \rho \delta(x) = (\nabla \cdot f) V$

then  $\int_V \nabla \cdot f dV = S$

but  $\int_V \nabla \cdot f dV = \int_A f \cdot n ds = \delta p A_b$

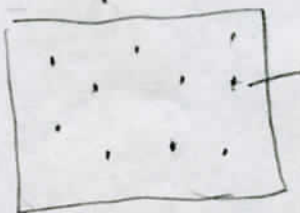
so  $S \approx \delta p A$

$$V = \frac{4}{3} \pi r^3$$

$$A = 4 \pi r^2$$

$$\frac{V}{A} = \frac{1}{3} r$$

$$\frac{A}{V^2} = \frac{4 \pi r^2}{\frac{16}{9} \pi^2 r^6} = \frac{9}{4 \pi r^4}$$



given  $\phi, V_b$

$$V_g = \phi V$$

$$N = \frac{\phi V}{V_b}$$

$$\overline{\nabla \cdot f} = \frac{1}{V} \int_V \nabla \cdot f dV = \frac{NS}{V}$$

$$= \frac{\phi V}{V_b} \frac{S}{V} = \frac{\phi S}{V_b}$$

$$= \phi \frac{A_b}{V_b} \delta p$$

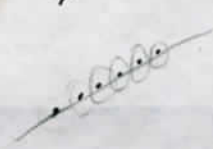
$$= \phi \frac{A_b}{V_b} \delta n RT$$

$$=$$

$\Sigma (x-x)$

$\frac{x}{V_b}$

$\oplus$





$$\ddot{u}_i = -\frac{1}{\rho} P_{,i}$$

$$-\ddot{u}_{i,i} = +\frac{1}{\rho} P_{,ii} \quad (\rho \text{ constant})$$

$$u_{k,k} = -\frac{P}{\lambda} = -cP$$

$$-\dot{u}_{k,k} = \dot{c}P + \dot{P}c$$

$$-\ddot{u}_{k,k} = c\ddot{P} + 2\dot{c}\dot{P} + \ddot{c}P$$

$$c\ddot{P} + 2\dot{c}\dot{P} + \ddot{c}P = \frac{1}{\rho} \nabla^2 P$$

$$\begin{aligned} \frac{d}{dt} &= \frac{dP}{dt} \frac{\partial}{\partial P} \\ \frac{d^2}{dt^2} &= \frac{dP}{dt} \frac{\partial}{\partial P} \frac{\partial}{\partial P} \frac{dP}{dt} \\ &= \left(\frac{dP}{dt}\right)^2 \frac{\partial^2}{\partial P^2} ? \end{aligned}$$

$$\dot{c} = \frac{\partial c}{\partial P} \dot{P}$$

$$\ddot{c} = \frac{\partial^2 c}{\partial P^2} \dot{P}^2$$

=

$$-\ddot{u}_{k,k} = \left(\frac{P}{\lambda}\right)'' = \frac{1}{\rho} \nabla^2 P$$

$$\begin{aligned} \nabla^2(cP) &= ((cP)_{,i})_{,i} = (cP_{,i} + c_{,i}P)_{,i} \\ &= cP_{,ii} + 2c_{,i}P_{,i} + c_{,ii}P \end{aligned}$$

$$\nabla^2(cP) = c\nabla^2 P + 2\nabla c \cdot \nabla P + P\nabla^2 c$$

$$\nabla^2 P = \frac{1}{c} \nabla^2(cP) - \frac{2}{c} \nabla c \cdot \nabla P - \frac{P}{c} \nabla^2 c$$

$$\nabla(cP) = c\nabla P + P\nabla c \quad \text{so} \quad \nabla P = \frac{1}{c} \nabla(cP) - \frac{P}{c} \nabla c$$

$$\nabla^2 P = \frac{1}{c} \nabla^2(cP) - \frac{2}{c^2} \nabla c \cdot \nabla(cP) + \frac{2(cP)}{c^3} \nabla c \cdot \nabla c - \frac{(cP)}{c^2} \nabla^2 c$$

$$P/\lambda = Q \quad P = \lambda Q$$

$$Q_3 - 2Q_2 + Q_1 = h^2 S$$

$$Q_3 = h^2 S + 2Q_2 - Q_1$$

$$P_3 = \lambda_3 Q_3$$

$$= (\lambda_2 + \lambda_1 t) Q_3$$

in gas

$$\tau_{ij} = -p \delta_{ij}$$

$$\epsilon_{ij} = d\delta_{ij} S_{ij} \quad \text{fluid}$$

$$\tau_{ij} = C_{ij} p \epsilon_{ij} = \lambda \delta_{ij} \epsilon_{pp} = -p \delta_{ij}$$

$$-p = \lambda \epsilon_{pp}$$

$$\epsilon_{pp} = \text{volumetric strain} = \frac{\Delta V}{V}$$

$$-\Delta p = \lambda \frac{\Delta V}{V}$$

$$-\frac{1}{V} \frac{\Delta V}{\Delta p} = \frac{1}{\lambda}$$

$$V = nRT p^{-1}$$

$$-\frac{1}{V} \frac{dV}{dp} = \frac{p}{nRT} nRT p^{-2} - \frac{p}{nRT p} \frac{dn}{dp}$$

$$\frac{1}{\lambda_b} = p^{-1} - \frac{1}{n} \frac{dn}{dp} = \frac{1}{p} \left( 1 - \frac{p}{n} \frac{dn}{dp} \right)$$

$$\lambda_b \approx p \left( 1 + \frac{p}{n} \frac{dn}{dp} \right) = p \left( 1 + \frac{1}{n} \frac{dn}{dt} / \frac{1}{p} \frac{dp}{dt} \right)$$

$$\lambda_T = \left( \frac{(1-\phi)}{\lambda_m} + \frac{\phi}{\lambda_s} \right)^{-1} \text{ say for mixture, so}$$

$$\int \frac{\partial^2 p}{\partial t^2} = \lambda_T(n, p) \frac{\partial^2 p}{\partial x^2}$$

$$\lambda_T = \left[ \frac{(1-\phi)}{\lambda_m} + \frac{\phi}{\lambda_b} \right]^{-1} \quad \text{and} \quad \frac{1}{\lambda_b} = p \left( 1 + \frac{1}{n} \frac{dn}{dt} / \frac{1}{p} \frac{dp}{dt} \right)$$

$$\frac{dn}{dt} = \begin{cases} a n_s(t) [P_s(t) - p(t)] & p < P_s \\ -b n(t) [p(t) - P_s(t)] & p \geq P_s \end{cases}$$

$$n_s(t) = n_t - n(t)$$

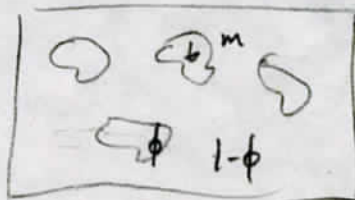
$$P_s(t) = P^* n_s(t) / n_s(t=0)$$

May 5, 2000

I have reviewed the proposal "Spontaneous Dynamic Rupture Sequences on Non-Planar Fault: Examining Segmentation Hypotheses of Hazard Estimates" by Bruce Shaw and find it worthy of submission.

Christopher Scholz  
Professor

$$-\frac{1}{V} \frac{dV}{dP} = \frac{1}{\lambda}$$



quasi-static  $\rightarrow$  dp same everywhere  
 $\phi$  = volume fraction of bubbles

$$dV_b = -\frac{V_b}{\lambda_b} dp = -\frac{\phi V_T}{\lambda_b} dp$$

$$dV_s = -\frac{V_m}{\lambda_m} dp = -\frac{(1-\phi)V_T}{\lambda_m} dp$$

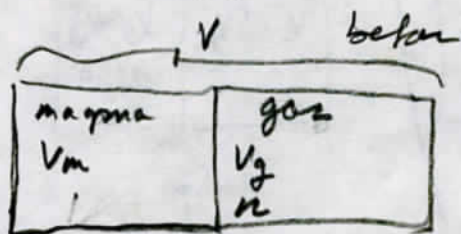
$$dV_T = (dV_b + dV_s) = -\left(\frac{\phi}{\lambda_b} + \frac{(1-\phi)}{\lambda_m}\right) V_T dp$$

$$\text{so } \lambda_T^{-1} = \left(\frac{\phi}{\lambda_b} + \frac{(1-\phi)}{\lambda_m}\right)$$

$$\begin{aligned} \lambda_T^{-1} &= \left(\frac{(1-\phi)}{\lambda_m} + \frac{\phi}{\lambda_b}\right)^{-1} = \frac{\lambda_m}{(1-\phi)} \left(1 + \frac{\lambda_m \phi}{\lambda_b (1-\phi)}\right)^{-1} \\ &= \frac{\lambda_m}{1-\phi} \left(1 - \frac{\phi}{(1-\phi)} \frac{\lambda_m}{P}\right) \end{aligned}$$

$$\frac{1}{V} \frac{\delta V}{\delta P} = -\frac{1}{\lambda}$$

$$\delta V = -\frac{V}{\lambda} \delta P$$

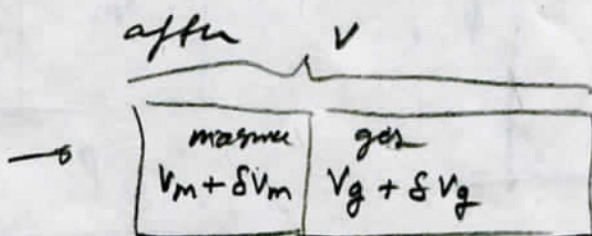


P

$$pV = nRT$$

$$(p + \delta p)(V + \delta V) = (n + \delta n)RT$$

$$V\delta p + p\delta V = \delta n RT$$



P +  $\delta P$

magma

$$\delta V_m = -\frac{V_m}{\lambda} \delta P$$

gas

$$p \delta V_g + V_g \delta p = \delta n RT$$

but  $\delta V_m = -\delta V_g$  and  $V_m = (1-\phi)V$  and  $V_g = \phi V$

$$\delta V_g = -\delta V_m = \frac{V_m}{\lambda_m} \delta P$$

$$P \frac{V_m}{\lambda_m} \delta P + p \frac{V_g}{P} \delta p = \delta n RT$$

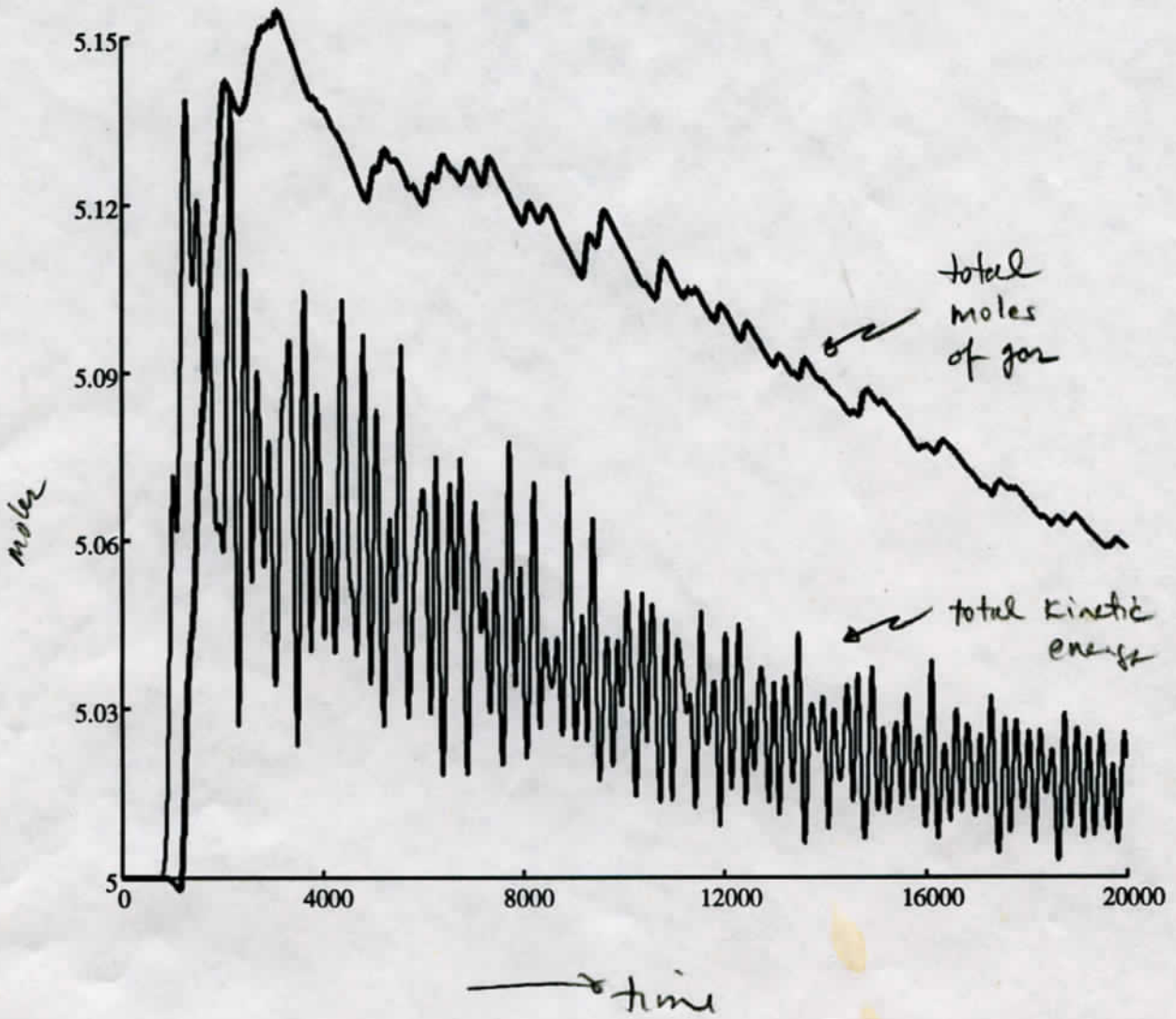
$$P \left( \frac{V_m}{\lambda_m} + \frac{V_g}{P} \right) \delta P = \delta n RT$$

$$P \delta P = \frac{\delta n RT}{\frac{V_m}{\lambda} + \frac{V_g}{P}} = \frac{\delta n RT}{V \left( \frac{1-\phi}{\lambda} + \frac{\phi}{P} \right)} = \frac{\frac{\delta n}{n} nRT}{\left( \frac{1-\phi}{\lambda} + \frac{\phi}{P} \right) V} = P \frac{\frac{\delta n}{n}}{\left( \frac{1-\phi}{\lambda} + \frac{\phi}{P} \right)}$$

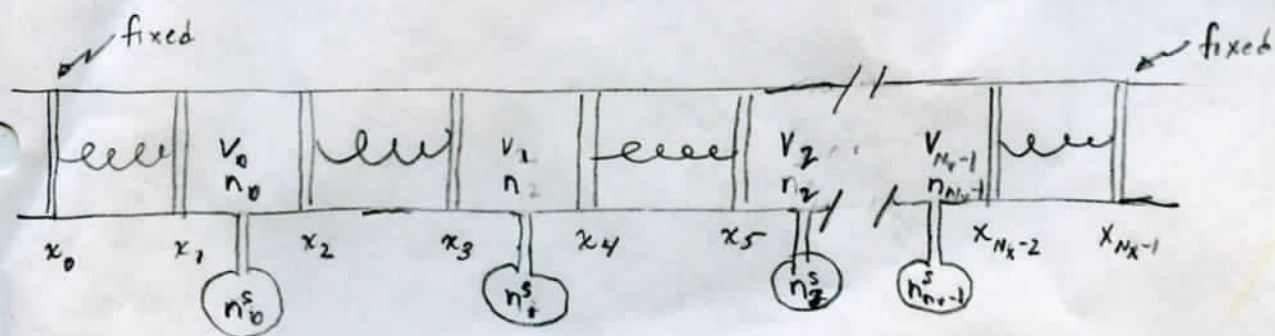
$$\delta P = \frac{\frac{\delta n}{n}}{\frac{1-\phi}{\lambda} + \frac{\phi}{P}}$$

$\lim_{\phi \rightarrow 1} \delta P = \frac{\delta n}{n}$

5e-3 1e-4



6 77 ek  
1 nt 79



$$\frac{dn}{dt} = \begin{cases} a \cdot n_s \cdot (P_s - P) & P_s \geq P \\ -b \cdot n \cdot (P - P_s) & P_s < P \end{cases} \quad \text{where } P_s = p^* \cdot n_s / n_s(0)$$

$P_s$  = vapor pressure of reservoir

Henry's law: vapor pressure proportional to mole fraction

Henry's law

$$p = K x$$

$$x = \text{mole fraction} = \frac{n}{n_{\text{ALL}}}$$

$$p = \frac{nK}{n_{\text{ALL}}}$$

compare ideal gas

$$p = n \frac{RT}{V}$$

$$\text{so } \frac{K}{n_{\text{ALL}}} = \frac{RT}{V}$$

so a box of  $n_{\text{ALL}}$  moles of Henry's Law solute is "equivalent" to a volume  $V = \frac{n_{\text{ALL}} RT}{K}$  of ideal gas.